

Amendments to the Claims:

1-130. (Cancelled)

131. (Previously presented) A process of producing a concentrated, stabilized liquid biocide formulation, which process consists of cofeeding to an aqueous solution formed from components consisting of water, sulfamic acid and alkali metal base, feed components consisting of (i) bromine and (ii) a solution of alkali metal base that maintains, while cofeeding, the pH of said concentrated, stabilized liquid biocide formulation produced in the range of from about 12 to about 14.

132. (Previously presented) A process according to claim 131 wherein said concentrated, stabilized liquid biocide formulation prepared in said step contains an amount of bromine that is no more than 26% of active bromine.

133. (Previously presented) A process according to claim 131 wherein said biocide formulation has an active bromine content of about 100,000 ppm (wt/wt) or more and an atom ratio of nitrogen to active bromine greater than 1.

134. (Previously presented) A process according to claim 131, wherein the pH is up to about 13.5.

135. (Currently amended) A process of producing a concentrated liquid biocide composition, which process consists ~~essentially~~ of

A) continuously feeding into mixing apparatus components consisting of (i) bromine and (ii) an aqueous solution of alkali metal salt of sulfamic acid having a pH of about 12 or more, proportioned to produce an aqueous product (a) having an active bromine content of at least 100,000 ppm (wt/wt), and an atom ratio of nitrogen to active bromine from (i) and (ii) greater than 1, and (b) maintaining the pH of said product in the range of from about 12 to about 14; and

B) withdrawing said product from said mixing apparatus at a rate sufficient to enable the continuous feeding in A) to be maintained.

136. (Previously presented) A process according to Claim 135 wherein (ii) in A) is an aqueous solution of the sodium salt of sulfamic acid.

137. (Previously presented) A process according to Claim 136 wherein said atom ratio is in the range of about 1.1 to about 1.5.

138. (Previously presented) A process according to Claim 135 wherein said mixing apparatus comprises a static mixer.

139. (Previously presented) A process according to Claim 135 wherein said mixing apparatus comprises a vessel equipped with a mechanical stirrer.

140. (Previously presented) A process according to Claim 139 wherein said product is intermittently withdrawn from said vessel.

141. (Previously presented) A process according to Claim 139 wherein said product is continuously withdrawn from said vessel.

142. (Currently amended) A process of producing a concentrated liquid biocide composition, which process consists essentially of

- A) continuously feeding into mixing apparatus components consisting of (i) a bromine stream and (ii) a separate feed stream of an aqueous solution of alkali metal salt of sulfamic acid having a pH of about 12 or more, in proportions that produce an aqueous product (a) having an active bromine content of at least 100,000 ppm (wt/wt), and an atom ratio of nitrogen to active bromine from (i) and (ii) greater than 1, and (b) maintaining the pH of said product in the range of from about 12 to about 14; and
- B) withdrawing said product from said mixing apparatus at a rate sufficient to enable the continuous feeding in A) to be maintained; and
- C) continuously, but alternately, withdrawing from at least one and then from at least one other of at least two reaction vessels, an aqueous solution of alkali metal salt of sulfamic acid at a rate that maintains said stream of (ii) in A), and during the time the solution is being withdrawn from said at least one of at least two reaction vessels, forming additional aqueous solution of alkali metal salt of sulfamic acid in said at least one other of at least two reaction vessels from which solution is not then being withdrawn

143. (Previously presented) A process according to Claim 142 wherein said aqueous solution of alkali metal salt of sulfamic acid is an aqueous solution of the sodium salt of sulfamic acid.

144. (Previously presented) A process according to Claim 142 wherein said aqueous solution of alkali metal wherein said atom ratio is in the range of about 1.1 to about 1.5.

145. (Previously presented) A process according to Claim 142 wherein said mixing apparatus comprises a static mixer.

146. (Previously presented) A process according to any of Claim 142 wherein said mixing apparatus comprises a vessel equipped with a mechanical stirrer.

147. (Previously presented) A process according to Claim 146 wherein in B) said aqueous product is intermittently withdrawn from said vessel.

148. (Previously presented) A process according to Claim 146 wherein in B) said aqueous product is continuously withdrawn from said vessel.

149. (Previously presented) A process according to Claim 142 wherein said mixing apparatus comprises a static mixer, and wherein said additional aqueous solution of alkali metal salt of sulfamic acid is formed from an alkali metal base, sulfamic acid, and water.

150. (Previously presented) A process according to Claim 142 wherein said mixing apparatus comprises a static mixer, wherein said aqueous solution of alkali metal salt of sulfamic acid is an aqueous solution of sodium sulfamate, and wherein said additional aqueous solution of alkali metal salt of sulfamic acid is formed from a water-soluble sodium base, sulfamic acid, and water.

151. (Previously presented) A process according to Claim 150 wherein said sodium base is an aqueous solution of sodium hydroxide, and wherein the sodium sulfamate is formed as an aqueous solution by charging to a reactor (i) an aqueous solution of sodium hydroxide, and (ii) a slurry of sulfamic acid in water, or (iii) separate charges of sulfamic acid and water, or (iv) both of (ii) and (iii).